

Performance assessment of up-flow anaerobic multi-staged reactor followed by auto-aerated immobilized biomass unit for treating polyester wastewater, with biogas production

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Publication Year	2024
Grant Number	IMSIU-2000651479
DOI link	10.1007/s13201-024-02129-y
<p>Abstract: Polyester manufacturing industries produce highly polluted effluents, containing organics, nutrients, trace metals, and 1,4-dioxane, requiring a high degree of treatment before being discharged into the water bodies. This study focused on removing complex pollutants from a diluted polyester industrial effluent (DPIE) via a cost-efficient anaerobic/aerobic combined system, with biogas recovery. The integrated pilot-scale system was composed of an up-flow anaerobic multi-staged reactor (UASR; $V = 41$ L) followed by an auto-aerated immobilized biomass (AIB; $V_{\text{sponge}} = 9.54$ L) unit and operated at a total organic loading rate (OLR) of 0.75 ± 0.16 g COD/L/d and pH of 7.14 ± 0.14 at 25 °C. The UASR achieved removal efficiencies of $17.82 \pm 3.14\%$ and $15.90 \pm 3.08\%$ for chemical oxygen demand (COD, total and soluble) and $15.83 \pm 4.68\%$ for total Kjeldahl nitrogen (TKN), with bio-CH_4 yield of 263.24 ± 31.98 mL/g COD. Adding the AIB unit improved the overall COD_{total}, COD_{soluble}, and TKN to $93.94 \pm 2.39\%$, $94.84 \pm 2.23\%$, and $75.81 \pm 3.66\%$, respectively. The $\text{NH}_4\text{-N}$ removal efficiency was $85.66 \pm 2.90\%$ due to the oxic/nitrification condition on the sponge's outer surface. The entire system also achieved $73.26 \pm 2.68\%$, $77.48 \pm 5.74\%$, and $81.26 \pm 6.17\%$ removals for Fe (3.93 ± 0.95 ppm), Zn (5.92 ± 2.32 ppm), and 1,4 dioxane (2.50 ± 0.61 ppm). Moreover, the UASR-AIB maintained removal efficiencies of $76.53 \pm 8.47\%$ and $77.51 \pm 7.38\%$ for total suspended solids (TSS: 335.95 ± 42.84 mg/L) and volatile suspended solids (VSS: 263.50 ± 36.94 mg/L). Regarding the DPIE toxicity level, the EC_{50} value increased from 12.9 to 39.4% after UASR/AIB application. The UASR's microbial community at the genus level demonstrated that the synergistic cooperation of solubilization, hydrolysis, acidogenesis, acetogenesis, and methanogenesis was responsible for the degradation of DPIE components.</p>	